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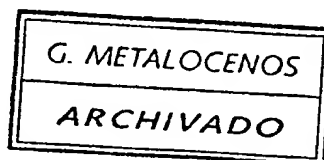
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Supported polymerization catalyst.

An olefin polymerization supported catalyst comprising a support and the reaction product of a metallocene of Group 4b, 5b or 6b of the Periodic Table and an alumoxane, said reaction product formed in the presence of a support.



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SUPPORTED POLYMERIZATION CATALYST

1           This invention relates to a new, improved catalyst useful  
2 for the polymerization and copolymerization of olefins and particu-  
3 larly useful for the polymerization of ethylene and copolymerization  
4 of ethylene with 1-olefins having 3 or more carbon atoms such as, for  
5 example, propylene, i-butene, 1-butene, 1-pentene, 1-hexene, and  
6 1-octene; dienes such as butadiene, 1,7-octadiene, and 1,4-hexadiene  
7 or cyclic olefins such as norbornene. The invention particularly  
8 relates to a new and improved heterogeneous transition metal contain-  
9 ing supported catalyst which can be employed without the use of an  
10 organometallic cocatalyst in the polymerization of olefins. The  
11 invention further generally relates to a process for polymerization  
12 of ethylene alone or with other 1-olefins or diolefins in the  
13 presence of the new supported transition metal containing catalyst  
14 comprising the reaction product of a metallocene and an alumoxane in  
15 the presence of an support material such as silica.

16 Description of the Prior Art

17           Traditionally, ethylene and 1-olefins have been polymerized  
18 or copolymerized in the presence of hydrocarbon insoluble catalyst  
19 systems comprising a transition metal compound and an aluminum  
20 alkyl. More recently, active homogeneous catalyst systems comprising  
21 a bis(cyclopentadienyl)titanium dialkyl or a bis(cyclopentadienyl)-  
22 zirconium dialkyl, an aluminum trialkyl and water have been found to  
23 be useful for the polymerization of ethylene. Such catalyst systems  
24 are generally referred to as "Ziegler-type catalysts".

25                     DE-A-2608863     discloses the use of a  
26 catalyst system for the polymerization of ethylene consisting of bis-  
27 (cyclopentadienyl) titanium dialkyl, aluminum trialkyl and water.

28                     DE-A-2608933     discloses an ethylene  
29 polymerization catalyst system consisting of zirconium metallocenes  
30 of the general formula  $(\text{cyclopentadienyl})_n \text{ZrY}_{4-n}$ , wherein n  
31 stands for a number in the range of 1 to 4, Y for  $\text{R}$ ,  $\text{CH}_2\text{AlR}_2$ ,  
32  $\text{CH}_2\text{CH}_2\text{AlR}_2$  and  $\text{CH}_2\text{CH}(\text{AlR}_2)_2$ , wherein R stands for alkyl or metallo  
33 alkyl, and an aluminum trialkyl cocatalyst and water.

34                     EP-A-0035242     discloses a process  
35 for preparing ethylene and atactic propylene polymers in the presence  
36 of a halogen-free Ziegler catalyst system of (1) cyclopentadienyl

1 compound of the formula  $(\text{cyclopentadienyl})_n \text{MeY}_{4-n}$  in which n is an  
2 integer from 1 to 4, Me is a transition metal, especially zirconium,  
3 and Y is either hydrogen, a  $\text{C}_1\text{-C}_5$  alkyl or metallo alkyl group or  
4 a radical having the following general formula  $\text{CH}_2\text{AlR}_2$ ,  $\text{CH}_2\text{CH}_2\text{AlR}_2$  and  
5  $\text{CH}_2\text{CH}(\text{AlR}_2)_2$  in which R represents a  $\text{C}_1\text{-C}_5$  alkyl or metallo alkyl  
6 group, and (2) an alumoxane.

7 Additional teachings of homogeneous catalyst systems com-  
8 prising a metallocene and alumoxane are  
9 EP-A-0069951, US 4404344 and EP-A-128045.

10  
11  
12  
13  
14 An advantage of the metallocene alumoxane homogeneous cata-  
15 lyst system is the very high activity obtained for ethylene polymeri-  
16 zation. Another significant advantage is, unlike olefin polymers  
17 produced in the presence of conventional heterogeneous Ziegler cata-  
18 lysts, terminal unsaturation is present in polymers produced in the  
19 presence of these homogeneous catalysts. Nevertheless, the catalysts  
20 suffer from a disadvantage, that is, the ratio of alumoxane to metal-  
21 locene is high, for example in the order of 1,000 to 1 or greater.  
22 Such voluminous amounts of alumoxane would require extensive treatment  
23 of polymer product obtained in order to remove the undesirable alumi-  
24 num. A second disadvantage, of the homogeneous catalyst system which  
25 is also associated with traditional heterogeneous Ziegler catalysts,  
26 is the multiple of delivery systems required for introducing the  
27 individual catalyst components into the polymerization reactor.

28 It would be highly desirable to provide a metallocene based  
29 catalyst which is commercially useful for the polymerization of ole-  
30 fins wherein the aluminum to transition metal ratio is within respect-  
31 able ranges and further to provide a polymerization catalyst which  
32 does not require the presence of a cocatalyst thereby reducing the  
33 number of delivery systems for introducing catalyst into polymeriza-  
34 tion reactor.

1 Summary of the Invention

2 In accordance with the present invention, a new metallocene/  
3 alumoxane catalyst is provided for olefin polymerization which cata-  
4 lyst can be usefully employed for the production of low, medium and  
5 high density polyethylenes and copolymers of ethylene with alpha-  
6 olefins having 3 to 18 or more carbon atoms and/or diolefins having up  
7 to 18 carbon atoms or more.

8 The new catalyst provided in accordance with one embodiment  
9 of this invention, comprises the reaction product of at least one  
10 metallocene and an alumoxane in the presence of an support material  
11 thereby providing a supported metallocene-alumoxane reaction product  
12 as the sole catalyst component.

13 The supported reaction product will polymerize olefins at  
14 commercially respectable rates without the presence of the objection-  
15 able excess of alumoxane as required in the homogenous system.

16 In yet another embodiment of this invention there is provided  
17 a process for the polymerization of ethylene and other olefins, and  
18 particularly homopolymers of ethylene and copolymers of ethylene and  
19 higher alpha-olefins and/or diolefins and/or cyclic olefins such as  
20 norbornene in the presence of the new catalysts.

21 The metallocenes employed in the production of the reaction  
22 product on the support are organometallic coordination compounds which  
23 are cyclopentadienyl derivatives of a Group 4b, 5b, or 6b metal of the  
24 Periodic Table (56th Edition of Handbook of Chemistry and Physics, CRC  
25 Press [1975]) and include mono, di and tricyclopentadienyls and their  
26 derivatives of the transition metals. Particularly desirable are the  
27 metallocene of a Group 4b and 5b metal such as titanium, zirconium,  
28 hafnium and vanadium. The alumoxanes employed in forming the reaction  
29 product with the metallocenes are themselves the reaction products of  
30 an aluminum trialkyl with water.

31 The alumoxanes are well known in the art and preferably comprise oligo-  
32 meric linear and/or cyclic alkyl alumoxanes represented by the formula:

1 (I)  $R-(Al-O)_n-AlR_2$  for oligomeric, linear alumoxanes and  
 2  $\quad \quad \quad |$   
 $\quad \quad \quad R$

3 (II)  $(-Al-O-)_m$  for oligomeric, cyclic alumoxane,  
 4  $\quad \quad \quad |$   
 $\quad \quad \quad R$

5 wherein n is 1-40, preferably 10-20, m is 3-40, preferably 3-20 and R  
 6 is a  $C_1-C_8$  alkyl group and preferably methyl. Generally, in the  
 7 preparation of alumoxanes from, for example, aluminum trimethyl and  
 8 water, a mixture of linear and cyclic compounds is obtained.

9 The alumoxanes can be prepared in a variety of ways. Prefer-  
 10 ably, they are prepared by contacting water with a solution of alumi-  
 11 num trialkyl, such as, for example, aluminum trimethyl, in a suitable  
 12 organic solvent such as benzene or an aliphatic hydrocarbon. For  
 13 example, the aluminum alkyl is treated with water in the form of a  
 14 moist solvent. In a preferred method, the aluminum alkyl, such as  
 15 aluminum trimethyl, can be desirably contacted with a hydrated salt  
 16 such as hydrated ferrous sulfate. The method comprises treating a  
 17 dilute solution of aluminum trimethyl in, for example, toluene with  
 18 ferrous sulfate heptahydrate.

#### 19 PREFERRED EMBODIMENTS

20 Briefly, the transition metal containing catalyst of the  
 21 present invention is obtained by reacting an alumoxane and a metal-  
 22 locene in the presence of a solid support material. The supported  
 23 reaction product can be employed as the sole catalyst component for  
 24 the polymerization of olefins or, in the alternative, it can be  
 25 employed with a organometallic cocatalyst.

26 Typically, the support can be any of the solid, particularly,  
 27 porous supports such as talc, inorganic oxides, and resinous support  
 28 materials such as polyolefin. Preferably, the support material is an  
 29 inorganic oxide in finely divided form.

30 Suitable inorganic oxide materials which are desirably  
 31 employed in accordance with this invention include Group 2a, 3a, 4a or  
 32 4b metal oxides such as silica, alumina, and silica-alumina and mix-  
 33 tures thereof. Other inorganic oxides that may be employed either  
 34 alone or in combination with the silica, alumina or silica-alumina are

1   magnesia, titania, zirconia, and the like. Other suitable support  
2   materials, however, can be employed, for example, finely divided  
3   polyolefins such as finely divided polyethylene.

4           The metal oxides generally contain acidic surface hydroxyl  
5   groups which will react with the alumoxane or transition metal com-  
6   pound first added to the reaction solvent. Prior to use, the inorganic  
7   oxide support may be dehydrated, ie subjected to a thermal treatment in  
8   order to remove water and reduce the concentration of the surface  
9   hydroxyl groups. The treatment may be carried out in vacuum or  
10  while purging with a dry inert gas such as nitrogen at a temperature  
11  of about 100°C to about 1000°C, and preferably, from about 300°C to  
12  about 800°C. Pressure considerations are not critical. The duration  
13  of the thermal treatment can be from about 1 to about 24 hours.  
14  However, shorter or longer times can be employed provided equilibrium  
15  is established with the surface hydroxyl groups.

16           Chemical dehydration as an alternative method of dehydration  
17  of the metal oxide support material can advantageously be employed.  
18  Chemical dehydration converts all water and hydroxyl groups on the  
19  oxide surface to inert species. Useful chemical agents are for  
20  example,  $\text{SiCl}_4$ ; chlorosilanes, such as trimethylchlorosilane,  
21  dimethyaminotrimethylsilane and the like. The chemical dehydration is  
22  accomplished by slurring the inorganic particulate material, such as,  
23  for example, silica in an inert low boiling hydrocarbon, such as, for  
24  example, hexane. During the chemical dehydration reaction, the silica  
25  should be maintained in a moisture and oxygen-free atmosphere. To the  
26  silica slurry is then added a low boiling inert hydrocarbon solution  
27  of the chemical dehydrating agent, such as, for example, dichlorodi-  
28  methylsilane. The solution is added slowly to the slurry. The  
29  temperature ranges during chemical dehydration reaction can be from  
30  about 25°C to about 120°C, however, higher and lower temperatures can  
31  be employed. Preferably, the temperature will be about 50°C to about  
32  70°C. The chemical dehydration procedure should be allowed to proceed  
33  until all the moisture is removed from the particulate support  
34  material, as indicated by cessation of gas evolution. Normally, the  
35  chemical dehydration reaction will be allowed to proceed from about 30  
36  minutes to about 16 hours, preferably 1 to 5 hours. Upon completion  
37  of the chemical dehydration, the solid particulate material is  
38  filtered under a nitrogen atmosphere and washed one or more times

1 with a dry, oxygen-free inert hydrocarbon solvent. The wash solvents,  
2 as well as the diluents employed to form the slurry and the solution  
3 of chemical dehydrating agent, can be any suitable inert hydrocarbon.  
4 Illustrative of such hydrocarbons are heptane, hexane, toluene, iso-  
5 pentane and the like.

6 The normally hydrocarbon soluble metallocenes and alumoxanes  
7 are converted to a heterogeneous supported catalyst by depositing said  
8 metallocenes and alumoxanes on the dehydrated support material. The  
9 order of addition of the metallocene and alumoxane to the support  
10 material can vary. For example, the metallocene (neat or dissolved in  
11 a suitable hydrocarbon solvent) can be first added to the support  
12 material followed by the addition of the alumoxane; the alumoxane and  
13 metallocene can be added to the support material simultaneously; the  
14 alumoxane can be first added to the support material followed by the  
15 addition of the metallocene. In accordance with the preferred embodi-  
16 ment of this invention the alumoxane dissolved in a suitable inert  
17 hydrocarbon solvent is added to the support material slurried in the  
18 same or other suitable hydrocarbon liquid and thereafter the metal-  
19 locene is added to the slurry.

20 The treatment of the support material, as mentioned above, is  
21 conducted in an inert solvent. The same inert solvent or a different  
22 inert solvent is also employed to dissolve the metallocenes and alum-  
23 oxanes. Preferred solvents include mineral oils and the various  
24 hydrocarbons which are liquid at reaction temperatures and in which  
25 the individual ingredients are soluble. Illustrative examples of  
26 useful solvents include the alkanes such as pentane, iso-pentane,  
27 hexane, heptane, octane and nonane; cycloalkanes such as cyclopentane  
28 and cyclohexane; and aromatics such as benzene, toluene, ethylbenzene  
29 and diethylbenzene. Preferably the support material is slurried in  
30 toluene and the metallocene and alumoxane are dissolved in toluene  
31 prior to addition to the support material. The amount of solvent to  
32 be employed is not critical. Nevertheless, the amount should be  
33 employed so as to provide adequate heat transfer away from the cata-  
34 lyst components during reaction and to permit good mixing.

35 The supported catalyst of this invention is prepared by  
36 simply adding the reactants in the suitable solvent and preferably  
37 toluene to the support material slurry, preferably silica slurried in  
38 toluene. The ingredients can be added to the reaction vessel rapidly

1 or slowly. The temperature maintained during the contact of the  
2 reactants can vary widely, such as, for example, from 0° to 100°C.  
3 Greater or lesser temperatures can also be employed. Preferably, the  
4 alumoxanes and metallocenes are added to the silica at room tempera-  
5 ture. The reaction between the alumoxane and the support material is  
6 rapid, however, it is desirable that the alumoxane be contacted with  
7 the support material for about one hour up to eighteen hours or  
8 greater. Preferably, the reaction is maintained for about one hour.  
9 The reaction of the alumoxane, the metallocene and the support  
10 material is evidenced by its exothermic nature and a color change.

11 At all times, the individual ingredients as well as the  
12 recovered catalyst component are protected from oxygen and moisture.  
13 Therefore, the reactions must be performed in an oxygen and moisture  
14 free atmosphere and recovered in an oxygen and moisture free atmos-  
15 phere. Preferably, therefore, the reactions are performed in the  
16 presence of an inert dry gas such as, for example, nitrogen. The  
17 recovered solid catalyst is maintained in a nitrogen atmosphere.

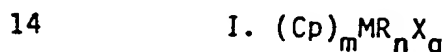
18 Upon completion of the reaction of the metallocene and alum-  
19 oxane with the support, the solid material can be recovered by any  
20 well-known technique. For example, the solid material can be recov-  
21 ered from the liquid by vacuum evaporation or decantation. The solid  
22 is thereafter dried under a stream of pure dry nitrogen or dried under  
23 vacuum.

24 The amount of alumoxane and metallocene usefully employed in  
25 preparation of the solid supported catalyst component can vary over a  
26 wide range. The concentration of the alumoxane added to the essen-  
27 tially dry, support can be in the range of about 0.1 to about 10  
28 mmols/g of support, however, greater or lesser amounts can be use-  
29 fully employed. Preferably, the alumoxane concentration will be in  
30 the range of 0.5 to 10 mmols/g of support and especially 1 to 5  
31 mmols/g of support. The amount of metallocene added will be such as  
32 to provide an aluminum to transition metal mole ratio of from about  
33 1:1 to about 100:1. Preferably, the ratio is in the range from about  
34 5:1 to about 50:1 and more preferably in the range from about 10:1 to  
35 about 20:1. These ratios are significantly less than that which is  
36 necessary for the homogeneous system.

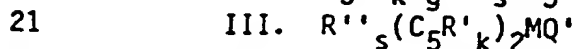
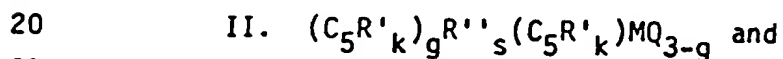


1           The present invention employs at least one metallocene com-  
 2 pound in the formation of the supported catalyst. Metallocene, i.e. a  
 3 cyclopentadienylide, is a metal derivative of a cyclopentadiene. The  
 4 metallocenes usefully employed in accordance with this invention  
 5 contain at least one cyclopentadiene ring. The metal is selected from  
 6 Group 4b, 5b and 6b metal, preferably 4b and 5b metals, preferably  
 7 titanium, zirconium, hafnium, chromium, and vanadium, and especially  
 8 titanium and zirconium. The cyclopentadienyl ring can be unsubsti-  
 9 tuted or contain substituents such as, for example, a hydrocarbyl  
 10 substituent. The metallocene can contain one, two, or three cyclo-  
 11 pentadienyl ring however two rings are preferred.

12           The preferred metallocenes can be represented by the general  
 13 formulas:



15 wherein Cp is a cyclopentadienyl ring, M is a Group 4b, 5b, or 6b  
 16 transition metal, R is a hydrocarbyl group or hydrocarboxy having from  
 17 1 to 20 carbon atoms, X is a halogen, and m = 1-3, n = 0-3, q = 0-3  
 18 and the sum of m+n+q will be equal to the oxidation state of the  
 19 metal.



22 wherein  $(C_5R'_k)$  is a cyclopentadienyl or substituted cyclopenta-  
 23 dienyl, each R' is the same or different and is hydrogen or a hydro-  
 24 carbyl radical such as alkyl, alkenyl, aryl, alkylaryl, or arylalkyl  
 25 radical containing from 1 to 20 carbon atoms or two carbon atoms are  
 26 joined together to form a C<sub>4</sub>-C<sub>6</sub> ring, R'' is a C<sub>1</sub>-C<sub>4</sub> alkylene  
 27 radical, a dialkyl germanium or silicon, or a alkyl phosphine or amine  
 28 radical bridging two  $(C_5R'_k)$  rings, Q is a hydrocarbyl radical  
 29 such as aryl, alkyl, alkenyl, alkylaryl, or aryl alkyl radical having  
 30 from 1-20 carbon atoms, hydrocarboxy radical having from 1-20 carbon  
 31 atoms or halogen and can be the same or different from each other, Q'  
 32 is an alkylidene radical having from 1 to about 20 carbon atoms, s is  
 33 0 or 1, g is 0, 1 or 2, s is 0 when g is 0, k is 4 when s is 1 and k  
 34 is 5 when s is 0, and M is as defined above.

35           Exemplary hydrocarbyl radicals are methyl, ethyl, propyl,  
 36 butyl, amyl, isoamyl, hexyl, isobutyl, heptyl, octyl, nonyl, decyl,  
 37 cetyl, 2-ethylhexyl, phenyl and the like.

1 Exemplary halogen atoms include chlorine, bromine, fluorine  
2 and iodine and of these halogen atoms, chlorine is preferred.

3 Exemplary hydrocarboxy radicals are methoxy, ethoxy, propoxy,  
4 butoxy, amyloxy and the like.

5 Exemplary of the alkylidene radicals is methyldiene, ethyldiene and propyldiene.

7 Illustrative, but non-limiting examples of the metallocenes  
8 represented by formula I are dialkyl metallocenes such as bis(cyclopentadienyl)titanium dimethyl, bis(cyclopentadienyl)titanium diphenyl,  
9 bis(cyclopentadienyl)zirconium dimethyl, bis(cyclopentadienyl)-  
10 zirconium diphenyl, bis(cyclopentadienyl)hafnium dimethyl and  
11 diphenyl, bis(cyclopentadienyl)titanium di-neopentyl, bis(cyclopentadienyl)zirconium di-neopentyl, bis(cyclopentadienyl)titanium dibenzyl,  
12 bis(cyclopentadienyl)zirconium dibenzyl, bis(cyclopentadienyl)vanadium  
13 dimethyl; the mono alkyl metallocenes such as bis(cyclopentadienyl)-  
14 titanium methyl chloride, bis(cyclopentadienyl)titanium ethyl  
15 chloride, bis(cyclopentadienyl)titanium phenyl chloride, bis(cyclopentadienyl)zirconium methyl chloride, bis(cyclopentadienyl)zirconium  
16 ethyl chloride, bis(cyclopentadienyl)zirconium phenyl chloride, bis-  
17 (cyclopentadienyl)titanium methyl bromide, bis(cyclopentadienyl)methyl  
18 iodide, bis(cyclopentadienyl)titanium ethyl bromide, bis(cyclopentadienyl)titanium ethyl iodide, bis(cyclopentadienyl)titanium phenyl  
19 bromide, bis(cyclopentadienyl)titanium phenyl iodide, bis(cyclopentadienyl)zirconium methyl bromide, bis(cyclopentadienyl)zirconium methyl  
20 iodide, bis(cyclopentadienyl)zirconium ethyl bromide, bis(cyclopentadienyl)zirconium ethyl iodide, bis(cyclopentadienyl)zirconium phenyl  
21 bromide, bis(cyclopentadienyl)zirconium phenyl iodide; the trialkyl  
22 metallocenes such as cyclopentadienyltitanium trimethyl, cyclopentadienyl zirconium triphenyl, and cyclopentadienyl zirconium trineo-  
23 pentyl, cyclopentadienylzirconium trimethyl, cyclopentadienylhafnium  
24 triphenyl, cyclopentadienylhafnium trineopentyl, and cyclopentadienyl-  
25 hafnium trimethyl.

33 Illustrative, but non-limiting examples of II and III metallocenes which can be usefully employed in accordance with this invention are monocyclopentadienyls titanocenes such as, pentamethylcyclopentadienyl titanium trichloride, pentaethylcyclopentadienyl titanium trichloride; bis(pentamethylcyclopentadienyl) titanium diphenyl, the carbene represented by the formula bis(cyclopentadienyl)titanium=CH<sub>2</sub>

1 and derivatives of this reagent such as bis(cyclopentadienyl)-  
 2  $\text{Ti}=\text{CH}_2\cdot\text{Al}(\text{CH}_3)_3$ ,  $(\text{Cp}_2\text{TiCH}_2)_2$ ,  $\text{Cp}_2\text{TiCH}_2\text{CH}(\text{CH}_3)\text{CH}_2$ ,  
 3  $\text{Cp}_2\text{Ti}-\text{CHCH}_2\text{CH}_2$ ; substituted bis(cyclopentadienyl)titanium (IV)  
 4 compounds such as: bis(indenyl)titanium diphenyl or dichloride, bis-  
 5 (methylcyclopentadienyl)titanium diphenyl or dihalides; dialkyl,  
 6 trialkyl; tetra-alkyl and penta-alkyl cyclopentadienyl titanium  
 7 compounds such as bis(1,2-dimethylcyclopentadienyl)titanium diphenyl  
 8 or dichloride, bis(1,2-diethylcyclopentadienyl)titanium diphenyl or  
 9 dichloride and other dihalide complexes; silicon, phosphine, amine or  
 10 carbon bridged cyclopentadiene complexes, such as dimethyl silyl-  
 11 dicyclopentadienyl titanium diphenyl or dichloride, methyl phosphine  
 12 dicyclopentadienyl titanium diphenyl or dichloride, methylenedi-  
 13 cyclopentadienyl titanium diphenyl or dichloride and other dihalide  
 14 complexes and the like.

15 Illustrative but non-limiting examples of the zirconocenes  
 16 Formula II and III which can be usefully employed in accordance with  
 17 this invention are, pentamethylcyclopentadienyl zirconium trichloride,  
 18 pentaethylcyclopentadienyl zirconium trichloride, bis(pentamethyl-  
 19 cyclopentadienyl)zirconium diphenyl, the alkyl substituted cyclopenta-  
 20 dienes, such as bis(ethyl cyclopentadienyl)zirconium dimethyl, bis-  
 21 ( $\beta$ -phenylpropylcyclopentadienyl)zirconium dimethyl, bis(methylcyclo-  
 22 pentadienyl)zirconium dimethyl, bis(n-butyl-cyclopentadienyl)zirconium  
 23 dimethyl, bis(cyclohexylmethylcyclopentadienyl)zirconium dimethyl,  
 24 bis(n-octyl-cyclopentadienyl)zirconium dimethyl, and haloalkyl and  
 25 dihalide complexes of the above; di-alkyl, trialkyl, tetra-alkyl, and  
 26 penta-alkyl cyclopentadienes, such as bis(pentamethylcyclopentadienyl)  
 27 zirconium di-methyl, bis(1,2-dimethylcyclopentadienyl)zirconium  
 28 dimethyl and dihalide complexes of the above; silicone, phosphorus,  
 29 and carbon bridged cyclopentadiene complexes such as dimethylsilyldi-  
 30 cyclopentadienyl zirconium dimethyl or dihalide, and methylene  
 31 dicyclopentadienyl zirconium dimethyl or dihalide, and methylene  
 32 dicyclopentadienyl zirconium dimethyl or dihalide, carbenes  
 33 represented by the formula  $\text{Cp}_2\text{Zr}=\text{CHP}(\text{C}_6\text{H}_5)_2\text{CH}_3$ , and derivatives of these  
 34 compounds such as  $\text{Cp}_2\text{ZrCH}_2\text{CH}(\text{CH}_3)\text{CH}_2$ .

35 Bis(cyclopentadienyl)hafnium dichloride, bis(cyclopenta-  
 36 dienyl)hafnium dimethyl, bis(cyclopentadienyl)vanadium dichloride and  
 37 the like are illustrative of other metallocenes.

1           the inorganic oxide support used in the preparation of the  
2 catalyst may be any particulate oxide or mixed oxide as previously  
3 described which has been thermally or chemically dehydrated such that  
4 it is substantially free of adsorbed moisture.

5           The specific particle size, surface area, pore volume, and  
6 number of surface hydroxyl groups characteristic of the inorganic  
7 oxide are not critical to its utility in the practice of the inven-  
8 tion. However, since such characteristics determine the amount of  
9 inorganic oxide that it is desirable to employ in preparing the cata-  
10 lyst compositions, as well as affecting the properties of polymers  
11 formed with the aid of the catalyst compositions, these character-  
12 istics must frequently be taken into consideration in choosing an  
13 inorganic oxide for use in a particular aspect of the invention. For  
14 example, when the catalyst composition is to be used in a gas-phase  
15 polymerization process - a type of process in which it is known that  
16 the polymer particle size can be varied by varying the particle size  
17 of the support - the inorganic oxide used in preparing the catalyst  
18 composition should be one having a particle size that is suitable for  
19 the production of a polymer having the desired particle size. In  
20 general, optimum results are usually obtained by the use of inorganic  
21 oxides having an average particle size in the range of about 30 to 600  
22 microns, preferably about 30 to 100 microns; a surface area of about  
23 50 to 1,000 square meters per gram, preferably about 100 to 400 square  
24 meters per gram; and a pore volume of about 0.5 to 3.5 cc per gram;  
25 preferably about 0.5 to 2cc per gram.

26           The polymerization may be conducted by a solution, slurry, or  
27 gas-phase technique, generally at a temperature in the range of about  
28 0°-160°C or even higher, and under atmospheric, subatmospheric, or  
29 superatmospheric pressure conditions; and conventional polymerization  
30 adjuvants, such as hydrogen may be employed if desired. It is  
31 generally preferred to use the catalyst compositions at a concentra-  
32 tion such as to provide about 0.000001 - 0.005%, most preferably about  
33 0.000001 - 0.0003%, by weight of transition metal based on the weight  
34 of monomer(s), in the polymerization of ethylene, alone or with one or  
35 more higher olefins.

36           A slurry polymerization process can utilize sub- or super-  
37 atmospheric pressures and temperatures in the range of 40-110°. In  
38 slurry polymerization, a suspension of solid, particulate catalyst

1 is formed in a liquid polymerization medium to which ethylene, alpha-  
2 olefin comonomer, hydrogen and catalyst are added. The liquid  
3 employed as the polymerization medium can be an alkane or cycloalkane,  
4 such as butane, pentane, hexane, or cyclohexane, or an aromatic hydro-  
5 carbon, such as toluene, ethylbenzene or xylene. The medium employe;  
6 should be liquid under the conditions of the polymerization and rela-  
7 tively inert. Preferably, hexane or toluene is employed.

8 A gas-phase polymerization process utilizes superatmospheric  
9 pressure and temperatures in the range of about 50°-120°C. Gas-phase  
10 polymerization can be performed in a stirred or fluidized bed of  
11 catalyst and product particles in a pressure vessel adapted to permit  
12 the separation of product particles from unreacted gases. Thermo-  
13 stated ethylene, comonomer, hydrogen and an inert diluent gas such as  
14 nitrogen can be introduced or recirculated so as to maintain the  
15 particles at a temperature of 50°-120°C. Triethylaluminum may be  
16 added as needed as a scavenger of water, oxygen, and other adventi-  
17 tious impurities. Polymer product can be withdrawn continuously or  
18 semi-continuing at a rate such as to maintain a constant product  
19 inventory in the reactor. After polymerization and deactivation of  
20 the catalyst, the product polymer can be recovered by any suitable  
21 means. In commercial practice, the polymer product can be recovered  
22 directly from the gas phase reactor, freed of residual monomer with a  
23 nitrogen purge, and used without further deactivation or catalyst  
24 removal. The polymer obtained can be extruded into water and cut into  
25 pellets or other suitable comminuted shapes. Pigments, antioxidants  
26 and other additives, as is known in the art, may be added to the  
27 polymer.

28 The molecular weight of polymer product obtained in accor-  
29 dance with this invention can vary over a wide range, such as low as  
30 500 up to 2,000,000 or higher and preferably 1,000 to about 500,000.

31 For the production of polymer product having a narrow molecu-  
32 lar weight distribution, it is preferable to deposit only one metal-  
33 locene on to the inert porous support material and employ said support  
34 metallocene together with the alumoxane as the polymerization cata-  
35 lyst.

1 It is highly desirable to have for many applications, such as  
2 extrusion and molding processes, polyethylenes which have a broad  
3 molecular weight distribution of the unimodal and/or the multimodal  
4 type. Such polyethylenes evidence excellent processability, i.e. they  
5 can be processed at a faster throughput rate with lower energy  
6 requirements and at the same time such polymers would evidence reduced  
7 melt flow perturbations. Such polyethylenes can be obtained by pro-  
8 viding a catalyst component comprising at least two different metal-  
9 locenes, each having different propagation and termination rate con-  
10 stants for ethylene polymerizations. Such rate constants are readily  
11 determined by one of ordinary skill in the art.

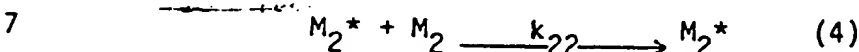
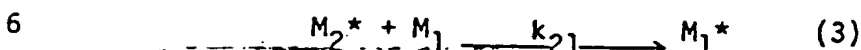
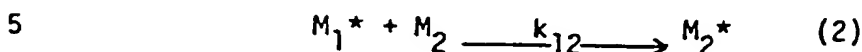
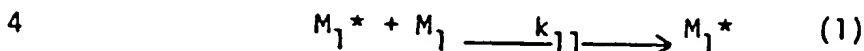
12 • The molar ratio of the metallocenes, such as, for example, of  
13 a zirconocene to a titanocene in such catalysts, can vary over a wide  
14 range, and in accordance with this invention, the only limitation on  
15 the molar ratios is the breadth of the Mw distribution or the degree  
16 of bimodality desired in the product polymer. Desirably, the metal-  
17 locene to metallocene molar ratio will be about 1:100 to about 100:1,  
18 and preferably 1:10 to about 10:1.

19 The present invention also provides a process for producing  
20 (co)polyolefin reactor blends comprising polyethylene and copoly-  
21 ethylene-alpha-olefins. The reactor blends are obtained directly  
22 during a single polymerization process, i.e., the blends of this  
23 invention are obtained in a single reactor by simultaneously poly-  
24 merizing ethylene and copolymerizing ethylene with an alpha-olefin  
25 thereby eliminating expensive blending operations. The process of  
26 producing reactor blends in accordance with this invention can be  
27 employed in conjunction with other prior art blending techniques, for  
28 example, the reactor blends produced in a first reactor can be sub-  
29 jected to further blending in a second stage by use of the series  
30 reactors.

31 In order to produce reactor blends the supported metallocene  
32 catalyst component comprises at least two different metallocenes each  
33 having different comonomer reactivity ratios.

34 The comonomer reactivity ratios of the metallocenes in  
35 general are obtained by well known methods, such as for example, as  
36 described in "Linear Method for Determining Monomer Reactivity Ratios  
37 in Copolymerization", M. Fineman and S. D. Ross, J. Polymer Science 5,  
38 259 (1950) or "Copolymerization", F. R. Mayo and C. Walling, Chem.

1 Rev. 46, 191 (1950) incorporated herein in its entirety by reference.  
 2 For example, to determine reactivity ratios the most widely used  
 3 copolymerization model is based on the following equations:



8 where  $M_i$  refers to a monomer molecule which is arbitrarily design-  
 9 nated  $i$  (where  $i = 1, 2$ ) and  $M_i^*$  refers to a growing polymer chain  
 10 to which monomer  $i$  has most recently attached.

11 The  $k_{ij}$  values are the rate constants for the indicated  
 12 reactions. In this case,  $k_{11}$  represents the rate at which an ethy-  
 13 lene unit inserts into a growing polymer chain in which the previously  
 14 inserted monomer unit was also ethylene. The reactivity rates follow  
 15 as:  $r_1 = k_{11}/k_{12}$  and  $r_2 = k_{22}/k_{21}$   
 16 wherein  $k_{11}$ ,  $k_{12}$ ,  $k_{22}$  and  $k_{21}$  are the rate constants for  
 17 ethylene (1) or comonomer (2) addition to a catalyst site where the  
 18 last polymerized monomer is ethylene ( $k_{1x}$ ) or comonomer (2) ( $k_{2x}$ ).

19 Since, in accordance with this invention, one can produce high  
 20 viscosity polymer product at a relatively high temperature, tempera-  
 21 ture does not constitute a limiting parameter as with the prior art  
 22 metallocene/alumoxane catalyst. The catalyst systems described  
 23 herein, therefore, are suitable for the polymerization of olefins in  
 24 solution, slurry or gas phase polymerizations and over a wide range of  
 25 temperatures and pressures. For example, such temperatures may be in  
 26 the range of about  $-60^\circ\text{C}$  to about  $280^\circ\text{C}$  and especially in the range of  
 27 about  $0^\circ\text{C}$  to about  $160^\circ\text{C}$ . The pressures employed in the process of  
 28 the present invention are those well known, for example, in the range  
 29 or about 1 to 500 atmospheres, however, higher pressures can be  
 30 employed.

31 The polymers produced by the process of this present inven-  
 32 tion are capable of being fabricated into a wide variety of articles,  
 33 as is known for homopolymers of ethylene and copolymers of ethylene  
 34 and higher alpha-olefins.

1 In a slurry phase polymerization, the alkyl aluminum scav-  
2 enger is preferably dissolved in a suitable solvent, typically in an  
3 inert hydrocarbon solvent such as toluene, xylene, and the like in a  
4 molar concentration of about  $5 \times 10^{-3}$  M. However, greater or lesser  
5 amounts can be used.

6 The present invention is illustrated by the following ex-  
7 amples.

#### 8 Examples

9 In the Examples following the alumoxane employed was prepared  
10 by adding 76.5 grams ferrous sulfate heptahydrate in 4 equally spaced  
11 increments over a 2 hour period to a rapidly stirred 2 liter round-  
12 bottom flask containing 1 liter of a 13.1 wt. % solution of trimethyl-  
13 aluminum (TMA) in toluene. The flask was maintained at 50°C and under  
14 a nitrogen atmosphere. Methane produced was continuously vented.  
15 Upon completion of the addition of ferrous sulfate heptahydrate the  
16 flask was continuously stirred and maintained at a temperature of 50°C  
17 for 6 hours. The reaction mixture was cooled to room temperature and  
18 was allowed to settle. The clear solution containing the alumoxane  
19 was separated by decantation from the insoluble solids.

20 Molecular weights were determined on a Water's Associates  
21 Model No. 150C-GPC (Gel Permeation Chromatography). The measurements  
22 were obtained by dissolving polymer samples in hot trichlorobenzene  
23 and filtered. The GPC runs are performed at 145°C in trichlorobenzene  
24 at 1.0 ml/min flow using styragel columns from Perkin Elmer, Inc.  
25 3.1% solutions (300 microliters of trichlorobenzene solution) were  
26 injected and the samples were run in duplicate. The integration  
27 parameters were obtained with a Hewlett-Packard Data Module.

#### 28 Catalyst Preparation

##### 29 Catalyst A

30 10 grams of a high surface area (Davison 952) silica, dehy-  
31 drated in a flow of dry nitrogen at 800°C for 5 hours, was slurried  
32 with 50 cc of toluene at 25°C under nitrogen in a 250 cc round-bottom  
33 flask using a magnetic stirrer. 25 cc of methyl alumoxane in toluene  
34 (1.03 moles/liter in aluminum) was added dropwise over 5 minutes with  
35 constant stirring to the silica slurry. Stirring was continued for 30  
36 minutes while maintaining the temperature at 25°C at which time the  
37 toluene was decanted off and the solids recovered. To the alumoxane  
38 treated silica was added dropwise over 5 minutes, with constant



1 stirring 25.0 cc of a toluene solution containing 0.200 gram of dicy-  
2 clopentadienyl zirconium dichloride. The slurry was stirred an addi-  
3 tional 1/2 hour while maintaining the temperature at 25°C and there-  
4 after the toluene was decanted and the solids recovered and dried in  
5 vacuo for 4 hours. The recovered solid was neither soluble nor  
6 extractable in hexane. Analysis of the catalyst indicated that it  
7 contained 4.5 wt. % aluminum and 0.63 wt. % zirconium.

#### 8 Catalyst B

9 This catalyst will demonstrate that the use of the catalyst  
10 of this invention in the production of copolyethylene with 1-butene  
11 results in the more efficient incorporation of 1-butene as demon-  
12 strated by the polymer product density.

13 The procedure for the preparation of Catalyst A was followed  
14 with the exception that the methylalumoxane treatment of the support  
15 material was eliminated. Analysis of the recovered solid indicated  
16 that it contained 0.63 wt. % zirconium and 0 wt. % aluminum.

#### 17 Catalyst C

18 The procedure for the preparation of Catalyst A was followed  
19 except that 0.300 of bis(cyclopentadienyl) zirconium dimethyl was  
20 substituted for the bis(cyclopentadienyl) zirconium dichloride.  
21 Analysis of the recovered solid indicated that it contained 4.2 wt. %  
22 aluminum and 1.1 wt. % zirconium.

#### 23 Catalyst D

24 The procedure for preparation of Catalyst A was followed with  
25 the exception that 0.270 g of bis(n-butyl-cyclopentadienyl) zirconium  
26 dichloride was substituted for the bis(cyclopentadienyl) zirconium  
27 dichloride of Catalyst A and all procedures were performed at 80°C.  
28 Analysis of the recovered solids indicated that it contained 0.61 wt.  
29 % zirconium and 4.3 wt. % aluminum.

#### 30 Catalyst E

31 The procedure for preparation of Catalyst D was followed with  
32 the exception that 0.250 grams of bis(n-butyl-cyclopentadienyl)-  
33 zirconium dimethyl was substituted for the metallocene dichloride.  
34 Analysis of the recovered solid indicated that it contained 0.63 wt %  
35 zirconium and 4.2 wt % aluminum.

1    Catalyst F

2            The procedure for the preparation of Catalyst D was followed  
3    with the exception that .500 grams of bis(pentamethylcyclopenta-  
4    dienyl)zirconium dichloride was substituted for the metallocene.  
5    Analysis of the recovered solid indicated that it contained 0.65 wt %  
6    zirconium and 4.7 wt % aluminum.

7    Example 1 - Polymerization - Catalyst A

8            Polymerization performed in the gas phase in a 1-liter auto-  
9    clave reactor equipped with a paddle stirrer, an external water jacket  
10   for temperature control, a septum inlet and a regulated supply of dry  
11   nitrogen, ethylene, hydrogen and 1-butene. The reactor, containing  
12   40.0 g of ground polystyrene (10 mesh) which was added to aid stirring  
13   in the gas phase, was dried and degassed thoroughly at 85°C. As a  
14   scavenger, 2.00 cc of a methyl alumoxane solution (0.64 molar in total  
15   aluminum) was injected through the septum inlet, into the vessel using  
16   a gas-tight syringe in order to remove traces of oxygen and water.  
17   The reactor contents were stirred at 120 rpm at 85°C for 1 minute at 0  
18   psig nitrogen pressure. 500.0 mg of Catalyst A was injected into the  
19   reactor and the reactor was pressured to 200 psig with ethylene. The  
20   polymerization was continued for 10 minutes while maintaining the  
21   reaction vessel at 85°C and 200 psig by constant ethylene flow. The  
22   reaction was stopped by rapidly cooling and venting. 12.3 grams of  
23   polyethylene were recovered. The polyethylene was recovered by  
24   stirring the product with 1 liter of dichloromethane at 40°C, filter-  
25   ing and washing with dichloromethane to recover the insoluble poly-  
26   ethylene product from the soluble polystyrene stirring aid. The  
27   polyethylene had a molecular weight of 146,000.

28   Example 2 - Polymerization - Catalyst A

29            Polymerization was performed as in Example 1 in the presence  
30   of Catalyst A except that 3.0 psig of hydrogen was pressured into the  
31   reactor prior to ethylene injection. 13.2 grams of polyethylene were  
32   recovered having a molecular weight of 29,000.

33   Example 3 - Polymerization - Catalyst A

34            Polymerization was performed as in Example 1 in the presence  
35   of Catalyst A except that 13.0 cc (0.137 moles) of 1-butene was  
36   pressured into the reactor together with the ethylene after the  
37   catalyst injection. 13.8 grams of polyethylene were recovered having  
38   a molecular weight of 39,000 and a density of 0.918 g/cc.

1 Comparative Example 3A - Polymerization - Catalyst B

2 The polymerization was performed as in Example 1 with the  
3 exception that Catalyst B was substituted for Catalyst A. 17.3 g of  
4 polyethylene were recovered having a molecular weight of 67,000 and a  
5 density of 0.935 g/cc. The higher density as compared with that  
6 obtained in Example 3 demonstrates the less efficient incorporation of  
7 comonomer.

8 Example 4 - Polymerization - Catalyst C

9 Polymerization was performed as in Example 1 with the excep-  
10 tion that Catalyst C was used in place of Catalyst A. 9.8 grams of  
11 polyethylene were recovered having a molecular weight of 189,000 and a  
12 density of 0.960 g/cc.

13 Example 5 - Polymerization - Catalyst C

14 Polymerization was performed as in Example 4 except that 13.0  
15 cc of 1-butene (0.123 moles) and 0.6 psig of hydrogen (1.66 milli-  
16 moles) was introduced after the catalyst together with the ethylene.  
17 6.5 grams of polyethylene were recovered having a molecular weight of  
18 41,000 and a density of 0.926 g/cc.

19 Example 6 - Polymerization - Catalyst C

20 Polymerization was performed as in Example 4, except that the  
21 scavenger methyl alumoxane was eliminated and no other aluminumalkyl  
22 scavenger was injected. 10.2 grams of polyethene was recovered having  
23 a molecular weight of 120,000 and a density of 0.960 g/cc.

24 Example 7 - Polymerization - Catalyst D

25 Polymerization was performed as in Example 1 with the excep-  
26 tion that 0.6 cc of a 25 wt. % triethylaluminum in hexane was substi-  
27 tuted for the methylalumoxane solution of Example 1, and Catalyst D  
28 was employed in place of Catalyst A. 50.4 g of polyethylene was  
29 recovered having a molecular weight of 196,000 and a density of 0.958  
30 g/cc.

31 Example 8 - Polymerization - Catalyst D

32 Polymerization was performed as in Example 1 with the excep-  
33 tion that the scavenger, methylalumoxane was eliminated, Catalyst D  
34 was employed in place of Catalyst A and the polymerization was stopped  
35 at the end of 5 minutes. 28.8 g of polyethylene was recovered having  
36 a molecular weight of 196,000 and a density of 0.958 g/cc.

1     Example 9 - Polymerization - Catalyst E

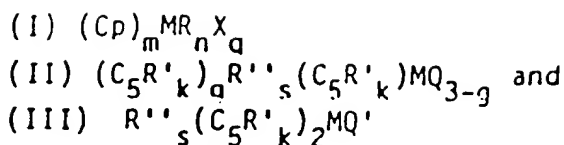
2             Polymerization was performed as in Example 8 using Catalyst E  
3     with no scavenger aluminum compound. 24.0 grams of polyethylene was  
4     recovered having a weight average molecular weight of 190,000, a  
5     number average molecular weight of 76,000 and a density of 0.958  
6     g/cc.

7     Example 10 - Polymerization - Catalyst F

8             Polymerization was performed as in Example 7 except that .500  
9     grams of Catalyst F was substituted for Catalyst D. 8.1 grams of  
10    polyethylene was recovered having a molecular weight of 137,000 and a  
11    density of 0.960 g/cc.

CLAIMS:

1. An olefin polymerization supported catalyst comprising the reaction product of at least one metallocene of a metal of Group 4b, 5b, and 6b of the Periodic Table and an alumoxane said reaction product formed in the presence of a support.
2. The olefin polymerization supported catalyst in accordance with claim 1 wherein the support is a porous inorganic metal oxide of a Group 2a, 3a, 4a or 4b metal.
3. The olefin polymerization supported catalyst in accordance with claim 2 wherein the support is silica.
4. The olefin polymerization supported catalyst in accordance with any of claims 1 to 3 wherein the metallocene is selected from titanium, zirconium, hafnium, and vanadium metallocenes and mixtures thereof.
5. The olefin polymerization supported catalyst in accordance with any of claims 1 to 4, wherein the alumoxane is methyl alumoxane.
6. The olefin polymerization supported catalyst in accordance with any of claims 1 to 5 wherein the aluminium to transition metal ratio in the supported product is in the range of 100:1 to 1:1 on a molar basis.
7. The olefin polymerization supported catalyst in accordance with claim 6 wherein the molar ratio is in the range of 50:1 to 5:1.
8. The olefin polymerization supported catalyst in accordance with claim 1 wherein the metallocenes are represented by the formulas



wherein Cp is a cyclopentadienyl ring, M is a Group 4b, 5b, or 6b transition metal, R is a hydrocarbyl group or hydrocarboxy having from 1 to 20 carbon atoms, X is a halogen,  $m=1-3$ ,  $n=0-3$ ,  $q=0-3$  and the sum of  $m + n + q$  is equal to the oxidation state of M,  $(\text{C}_5\text{R}'_k)$  is a cyclopentadienyl or a substituted cyclopentadienyl; each R' is the same or different and is hydrogen or a hydrocarbyl radical selected from alkyl, alkenyl, aryl, alkylaryl or arylalkyl radicals containing from 1 to 20 carbon atoms, or a link between two carbon atoms joined together to form a  $\text{C}_4\text{-C}_6$  ring, R'' is a  $\text{C}_1\text{-C}_4$  alkylene radical, a dialkyl germanium or silicon or an alkyl phosphine or amine radical bridging two  $(\text{C}_5\text{R}'_k)$  rings; Q is a hydrocarbyl radical selected from aryl, alkyl, alkenyl, alkylaryl, or arylalkyl radicals having from 1-20 carbon atoms, hydrocarboxy radical having from 1-20 carbon atoms or halogen and each Q can be the same or different from each other; Q' is an alkylidene radical having from 1 to about 20 carbon atoms; s is 0 or 1; g is 0, 1, or 2; s is 0 when g is 0; k is 4 when s is 1 and k is 5 when s is 0.

9. The olefin polymerization supported catalyst in accordance with claim 8 wherein the metallocenes are selected from bis-(cyclopentadienyl) zirconium dichloride, bis(cyclopentadienyl)-zirconium methyl chloride, bis(cyclopentadienyl) zirconium dimethyl, bis(methylcyclopentadienyl)zirconium dichloride, bis(methylcyclopentadienyl)zirconium methyl chloride, bis(methylcyclopentadienyl)zirconium dimethyl, bis(pentamethylcyclopentadienyl)zirconium dichloride, bis(pentamethylcyclopentadienyl)zirconium methyl chloride, bis(pentamethylcyclopentadienyl)zirconium dimethyl, bis(n-butyl-cyclopentadienyl) zirconium dichloride, bis(n-butylcyclopentadienyl)zirconium methyl chloride, bis(n-butyl-cyclopentadienyl)zirconium dimethyl, bis(cyclopentadienyl)titanium diphenyl, bis(cyclopentadienyl)titanium dichloride, bis(cyclopentadienyl)titanium methyl chloride, bis(cyclopentadienyl)titanium dimethyl, bis(methylcyclopentadienyl)titanium

diphenyl, bis(methylcyclopentadienyl) titanium dichloride, bis(methylcyclopentadienyl)- titanium diphenyl, bis(methylcyclopentadienyl)- titanium methyl chloride, bis(methylcyclopentadienyl)titanium dimethyl, bis(pentamethylcyclopentadienyl)titanium dichloride, bis-(pentamethylcyclopentadienyl)titanium diphenyl, bis(pentamethylcyclopentadienyl)titanium methyl chloride, bis(pentamethylcyclopentadienyl)titanium dimethyl, bis(n-butyl-cyclopentadienyl)titanium diphenyl, bis(n-butyl-cyclopentadienyl)titanium dichloride and mixtures thereof.

10. A method for preparing an olefin polymerization supported catalyst comprising a support and the reaction product of at least one metallocene of a metal of Group 4b, 5b and 6b of the Periodic Table and an alumoxane, comprising adding to a slurry of the support in an inert hydrocarbon solvent an alumoxane in an inert hydrocarbon solvent and a metallocene.

11. A method for preparing polymers of ethylene or copolymers of ethylene and alpha olefins or diolefins said method comprising effecting the polymerization in the presence of the olefin polymerization catalyst of any of claims 1 to 9.



European Patent  
Office

# EUROPEAN SEARCH REPORT

0206794

Application number

EP 86 30 4806

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 4)
D, A	EP-A-0 128 045 (EXXON) * Claims; page 9, lines 26-31 *	1	C 08 F 4/76 C 08 F 10/00
D, A	EP-A-0 035 242 (SINN HANSJÖRG) * Claims *	1	
			TECHNICAL FIELDS SEARCHED (Int. Cl. 4)
			C 08 F
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 22-09-1986	Examiner DE ROECK R.G.
CATEGORY OF CITED DOCUMENTS			
X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document		T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family corresponding document	